





On-Demand Reactivity Enhancement to Enable Advanced Low Temperature Natural Gas Internal Combustion Engines

Will Northrop – Principal Investigator Annual Merit Review and Peer Evaluation Meeting June 10-13, 2019

Project ID: ft086

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Project Overview

Timeline

Project Start Date: 5/1/2018

Project End Date: <u>6/30/2021</u>

Percent Complete: 25%

Budget

Total Project Funding:

DOE Share = \$1,102,367

Contractor = \$294,358

FY 2018 Funding = \$25,334

FY 2019 Funding* = \$173,599

Barriers

Lean/Dilute Natural Gas Combustion:

- Methane is a highly stable fuel requires high ignition energy in lean/dilute conditions
- Cannot be easily used in any advanced compression ignition modes
- Poor low temperature oxidation of methane in existing exhaust aftertreatment catalysts

Partners



University of Minnesota







^{*} through 5/1/2019

Relevance/Objectives

Overall Objectives

Demonstrate ≥10% indicated efficiency improvement compared to state-of-the-art lean-burn Natural Gas (NG) dedicated spark ignition (DSI) engine by using fuel pretreatment by oxidative coupling of methane (OCM)

Objectives in this Period

Experiments and modeling to demonstrate capability of the short contact time reactor to achieve desired OCM conversion and selectivity

Milestones

Tasks/Milestones	Budget Period 1				1	Budget Period 2				Budget Period 3			
	FY18		FY19					FY20		FY2		FY21	
	Q	Q2	Q3	Q 4	Q5	Q6	۵7	Q8	Q9	Q10	Q11	Q12	Q13
Perform Bench-Scale Short-Contact Reactor Studies (UMN)		M1.1			M1.2, D1.1							M1.3	
Develop Highly Effective OCM Catalysts and Wash-Coat Technology (JM)			M2.1				M2.2						
Design and Characterize Single Cylinder Engine and Reactor System (All)							M3.1	M3.2	M3.3, D3.1		M3.4		M3.5
4. Use CFD Modeling to Guide Reactor Design and LTCI Engine Combustion (CMU)			M4.1		M4.2			M4.3			M4.4	M4.5	
5. Prove NG Engine Efficiency Gains Through 1-D Modeling											M5.1		M5.2
		Completed			To be Completed				Current				

Approach

- Oxidative coupling of methane introduction
 - Proposed industrially to produce ethylene from natural gas
 - Low conversion and potential for unselective oxidation
 - Oxygen utilization is a challenge leads to unselective oxidation
 - Could be used to enhance the reactivity of natural gas for engines

Selective oxidation

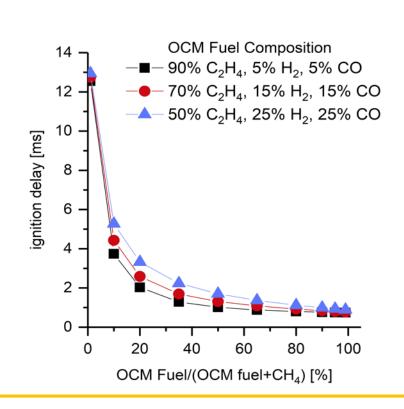
$$2CH_4 + \frac{1}{2}O_2 \to C_2H_6 + H_2O$$

$$C_2H_6 + \frac{1}{2}O_2 \rightarrow C_2H_4 + H_2O$$

<u>Unselective oxidation</u>

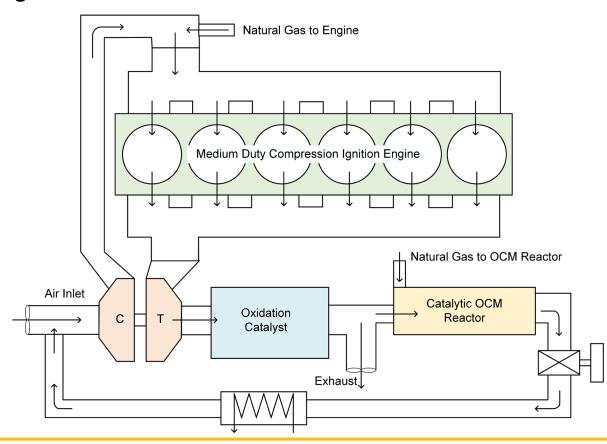
$$CH_4 + O_2 \rightarrow CO + H_2O + H_2$$

$$CH_4 + 2O_2 \rightarrow CO_2 + 2H_2O$$



Approach

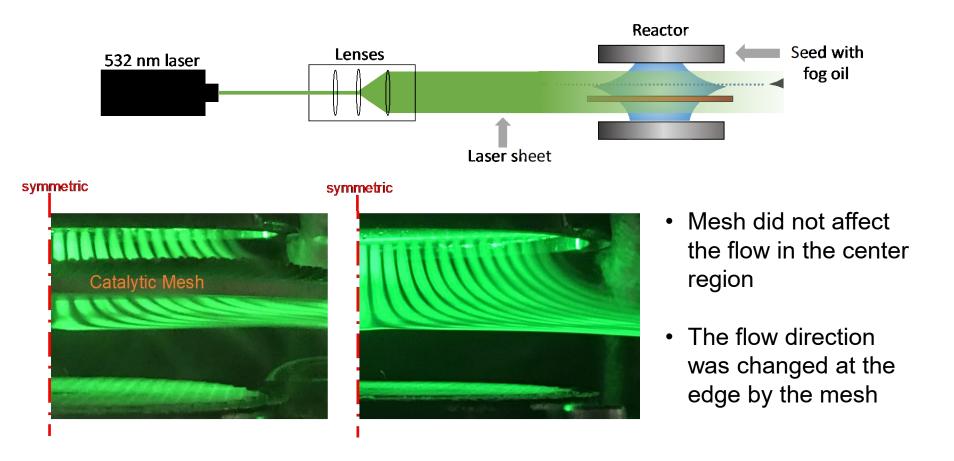
- Integrate OCM into a reformed exhaust gas recirculation scheme to enable advanced dilute combustion modes
- Use new short-contact time reactor to avoid oxygen utilization problems found in large-scale reactors



Task 1: Bench scale reactor completed and partial oxidation reforming catalyst tested

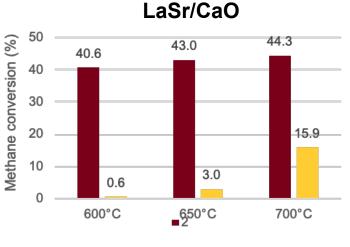
Derived from previous work under NSF project Premixed CH₄ & Air Inlet Opposed flow reactor avoids oxygen distribution problem in OCM Nitrogen Purge Partial oxidation experiments conducted Premixed CH₄ & Air Oxidation Catalyst Stagnation Plane • Flow Straightener Reforming Catalyst CH₄ Water Jacket

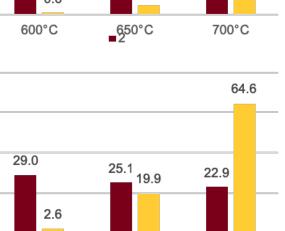
Task 1: Flow visualized to determine pressure drop through catalytic mesh

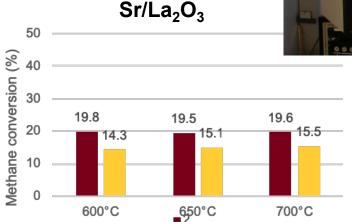


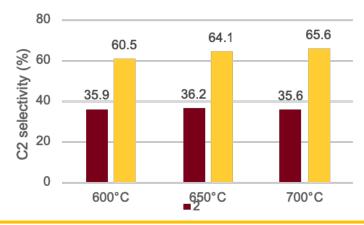
Task 2: Catalysts evaluated: integral micro-reactor

- Sr/La₂O₃ catalyst: better low temperature conversion
- Coated meshes provided for opposed flow reactor













Sr/La₂O₃ Mesh

Testing conditions

Space velocity 50,000 to 100,000 h⁻ CH₄/O₂ ratio from 2:1 to 6:1 molar Temperature 600-700°C

Presented here

Space velocity 50,000 h⁻¹ CH₄/O₂ ratio 2:1 or 6:1 molar Temperature 600-700°C

2:1 CH_4/O_2 lean 6:1 CH_4/O_2 rich



600°C

80

C2 selectivity (%)

_650°C

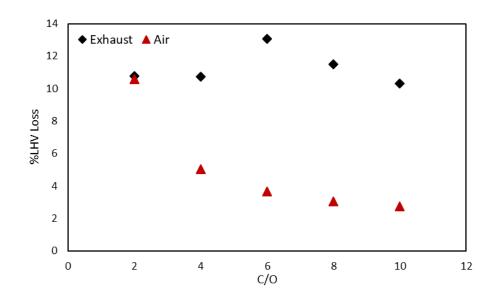
700°C

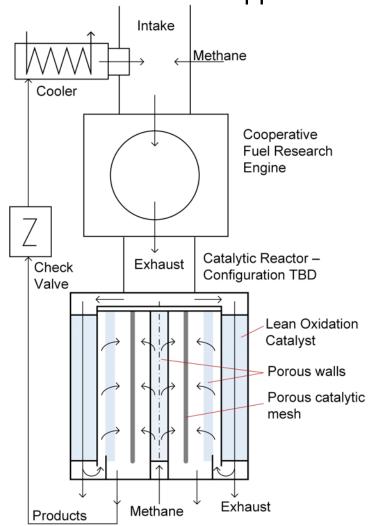
Task 3: Two approaches for engine scale reactor considered: opposed flow

and traditional monolith reactors

CFR reactor set up to study autoignition

- Short contact, better O₂ utilization
- Residence time may not be sufficient
- Rich reaction with fresh air may be required to mitigate LHV loss

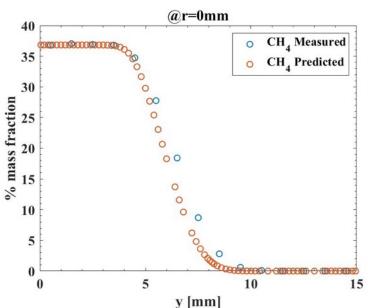


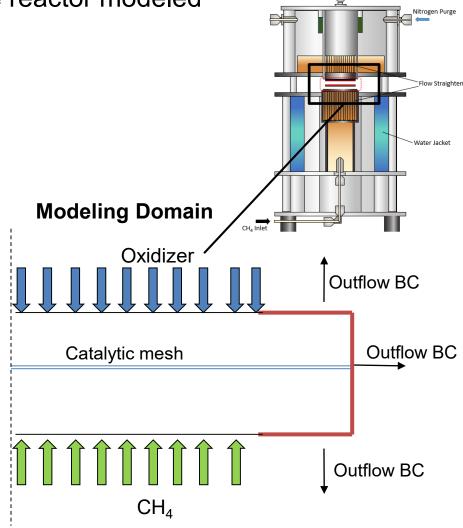


Task 4: Bench-scale short contact time reactor modeled in Fluent and Converge

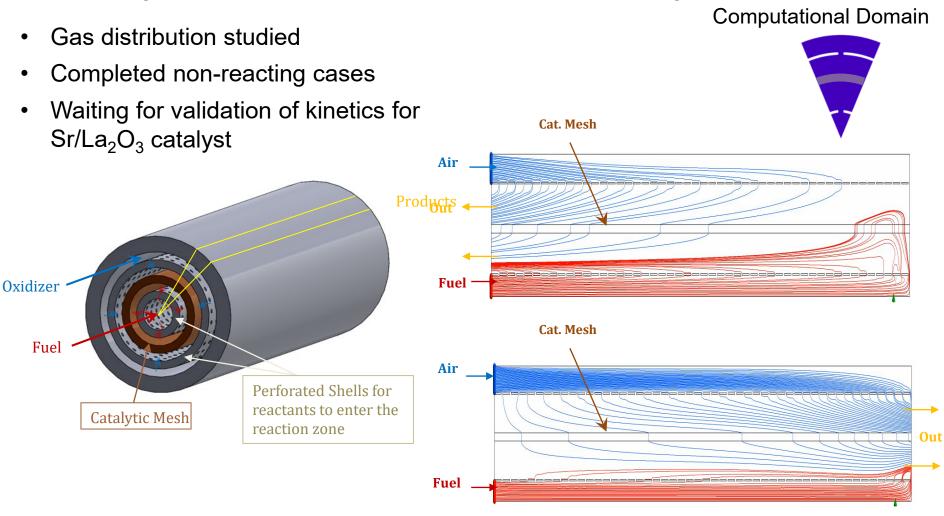
- Reacting and non-reacting cases modeled
- Reacting cases use literature partial oxidation mechanism

Non-Reacting CH₄ Comparison





Task 4: Engine-scale CFD model constructed in Converge



Response to Previous Comments

This is the first year the project has been presented

Partnerships/Collaborations





Partners

- OCM catalyst research and development
- Catalyst wash-coating for bench and engine-scale reactors
- Computational fluid dynamics of reactors and engines
- Supporting low-dimensional engine modeling efforts

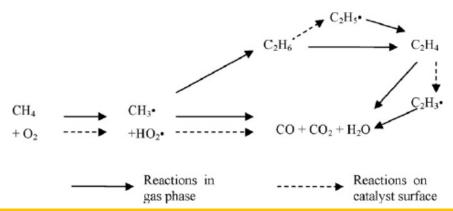


Collaborators

Provided OCM kinetics for modeling efforts

Remaining Challenges and Barriers

- Achieving acceptable conversion and selectivity over provided OCM catalysts using bench-scale reactor
- OCM reaction is more difficult than reforming:
 - Deactivation at T > 900°C
 - Low activity at T < 600°C
- Determine appropriate OCM stoichiometry to limit heating value loss balance with engine efficiency gain
- Short contact time may not achieve sufficient conversion of methane –
 OCM consists of series of gas + surface phase reactions¹



Proposed Future Research

To be completed in FY19/FY20(Q1):

- Characterize OCM in bench scale reactor, achieving >10% conversion and >20% selectivity to C₂ products
- Determine direction for engine-scale reactor design, short contact or monolith
- Configure single-cylinder engine test cell to begin engine reactivity studies

Future*:

 Should project be successful, the project team will seek opportunities to integrate with full scale natural gas engine

*Any proposed future work is subject to change based on funding levels

Thank You

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